**AMENDMENTS TO THE CLAIMS:**

This listing of claims will replace all prior versions, and listings, of claims in the application:

**LISTING OF CLAIMS:**

1. - 27. (Canceled).

28. (Currently Amended) A process for preparing a low water-uptake precipitated silica, comprising the following successive steps:

(a) producing an initial feedstock comprising a silicate, the silicate concentration in the feedstock, expressed in $SiO_2$ equivalent, being less than 15 g/l;

(b) adding an acidifying agent to form an acidified feedstock, bringing the pH of the medium to a value of between 7 and 8;

(c) ~~in the resulting medium,~~ simultaneously adding a silicate and an acidifying agent to the feedstock resulting from step (b) to form a reaction medium, the respective amounts of added silicate and acidifying agent over time being specifically selected such that, throughout the entire addition:

- the pH of the reaction medium remains between 7 and 8;
- the silicon concentration in the reaction medium, expressed in $SiO_2$ equivalent, remains less than or equal to 35 g/l;

(d) adding an acidifying agent to the reaction medium resulting from step (c), so as to bring the reaction medium [[at]] to a pH of between 3 and 6.5; and

(e) filtering the resulting aqueous silica dispersion, then drying the filter cake obtained at the end of the filtering step.

29. (Previously Presented) The process of claim 28, wherein the silicates used in steps (a) and (c) are alkali silicates.

30. (Previously Presented) The process of claim 28, wherein the acidifying agents used in steps (b), (c) and (d) comprise sulfuric acid, hydrochloric acid, nitric acid, acetic acid, formic acid and carbonic acid.

31. (Previously Presented) The process of claim 28, wherein the feedstock of step (a) is in the form of an aqueous silicate solution, having a concentration, expressed in $SiO_2$ equivalent, of less than or equal to 10 g/l.

32. (Previously Presented) The process of claim 28, wherein the acidifying agent of step (b) is introduced in the form of an aqueous solution having a normality of between 0.25 N and 8 N.

33. (Previously Presented) The process of claim 28, wherein the acidifying agent of step (b), is sulfuric acid, introduced in the form of an aqueous solution having a concentration of between 10 g/l and 350 g/l.

34. (Currently Amended) The process of claim 28, wherein the simultaneous addition of the silicate and acidifying agent of step (c) is carried out by continuously adding silicate to the reaction medium, the pH being adjusted during the addition by introducing acidifying agent if the pH of the medium becomes greater than a given control value, of between 7 and 8.

35. (Previously Presented) The process of claim 28, wherein the simultaneous addition of the silicate and acidifying agent of step (c) is carried out by continuously adding silicate to the medium, the pH being adjusted during the addition by introducing silicate if the pH of the medium becomes less than a test value of between 7 and 8.

36. (Currently Amended) The process of claim 28, wherein the simultaneous addition of the silicate and acidifying agent of step (c) comprises in continuously adding both acidifying agent and silicate, with concentrations and flow

rates calculated such that, throughout the addition, the pH of the reaction medium remains between 7 and 8.

37. (Previously Presented) The process of claim 28, wherein the silicate that is introduced during the simultaneous addition of step (c) is in the form of an aqueous solution having a concentration of between 10 g/l and 360 g/l.

38. (Previously Presented) The process of claim 28, wherein the acidifying agent that is introduced during the simultaneous addition of step (c) is in the form of an aqueous solution having a normality of between 0.25 N and 8 N.

39. (Previously Presented) The process of claim 28, wherein the addition of step (c) last between 15 and 300 minutes.

40. (Previously Presented) The process of claim 28, wherein an aluminum compound is introduced to the medium at the end of step (c), and/or between step (c) and step (e).

41. (Previously Presented) The process of claim 28, wherein step (d) is used, and in that the acidifying agent from step (d) is introduced to the medium in the form of an aqueous solution having a normality of between 0.25 N and 8.

42. (Previously Presented) The process of claim 28, wherein steps (a), (b) (c) and (d) are carried out at a temperature of between 90 and 100°C.

43. (Previously Presented) The process of claim 28, wherein the aqueous silica dispersion resulting from step (d) is subjected to a maturation step, prior to step (e).

44. (Previously Presented) The process of claim 28, wherein step (e) comprises a process of splitting the precipitate cake.

45. (Withdrawn) A silica obtained by the process of claim 28.

46. (Withdrawn) The silica of claim 45 having a water-uptake of less than 6%.

47. (Withdrawn) A silicone-based matrix in combination with a reinforcing filler, the filler comprising the silica of claim 45.

48. (Canceled)

49. (Withdrawn) A matrix based on one or more elastomers in combination with a reinforcing filler, the filler comprising the silica of claim 45.

50. (Withdrawn) The combination of claim 49, wherein said matrix based on one or more elastomers is a transparent or translucent matrix.

51. - 54. (Canceled)

55. (Withdrawn) An article comprising the silica of claim 45, the article comprising one or more of: a thickening agent, a food composition, a cosmetic composition, and a pharmaceutical composition.

56. (New) the process of claim 28, wherein in step (c) the pH is substantially constant around a fixed value.

57. (New) The process of claim 56, wherein in step (c) the pH is maintained within +/- 0.2 pH units of the fixed value.

58. (New) The process of claim 57, wherein the fixed value is 7.2 - 7.8.

59. (New) The process of claim 58, wherein the fixed value is 7.3 - 7.7.

60. (New) The process of claim 28, wherein throughout step (c) the following relationship is maintained:

$d_S/d_A = 1.01 - 1.09$;

wherein,

$d_S$ = amount of silicate functions expressed as molar equivalent of NaOH introduced per second; and

$d_A$ = amount of acid functions, in moles, introduced per second.

the fixed value is 7.2 - 7.8.